

METHOD FOR MAKING HIGH THERMAL DIFFUSIVITY BORON NITRIDE POWDERS

FIELD OF THE INVENTION

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The present invention relates to a method for making high thermal diffusivity boron nitride powders and the resulting powders.

BACKGROUND OF THE INVENTION

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Integrated circuit chips are steadily becoming smaller and more powerful. The current trend is to produce integrated chips which are steadily increasing in density and perform many more functions in a given period of time over predecessor chips. This results in an increase in the electrical current used by these
15 integrated circuit chips. As a result, these integrated circuit chips generate more ohmic heat than the predecessor chips. Accordingly, heat management has become a primary concern in the development of electronic devices.

Typically, heat generating sources or devices, such as, integrated circuit chips, are mated with heat sinks to remove heat which is generated during their
20 operation. However, thermal contact resistance between the source or device and the heat sink limits the effective heat removing capability of the heat sink. During assembly, it is common to apply a layer of thermally conductive grease, typically a silicone grease, or a layer of a thermally conductive organic wax to aid in creating a low thermal resistance path between the opposed mating surfaces of the heat source
25 and the heat sink. Other thermally conductive materials are based upon the use of a binder, preferably a resin binder, such as, a silicone, a thermoplastic rubber, a urethane, an acrylic, or an epoxy, into which one or more thermally conductive fillers are distributed.

Typically, these fillers are one of two major types: thermally
30 conductive, electrically insulative or thermally conductive, electrically conductive fillers. Aluminum oxide, magnesium oxide, zinc oxide, aluminum nitride, and boron nitride are the most often cited types of thermally conductive, electrically insulative fillers used in thermal products. Boron nitride is especially useful in that it has excellent heat transfer characteristics and is relatively inexpensive.

However, in order to achieve sufficient thermal conductivity with presently used fillers, such as boron nitride, it has been necessary to employ high loadings of filler in the binder (see, e.g., U.S. Patent No. 5,898,009 to Shaffer et al. and U.S. Patent No. 6,048,511 to Shaffer et al.). Thus, there is a need for thermally
5 conductive filler materials which can be used at low loading levels to achieve sufficient thermal conductivity. The present invention is directed to overcoming this deficiency in the art.

SUMMARY OF THE INVENTION

10 The present invention relates to a method for making boron nitride powder having a thermal diffusivity of from about $0.14 \text{ cm}^2/\text{s}$ to about $0.20 \text{ cm}^2/\text{s}$. This method involves pressing high purity, hexagonal boron nitride having an average platelet size of at least 2 microns into a compacted form, sintering the compacted
15 form of boron nitride to form a sintered body, and crushing the sintered body under conditions effective to produce boron nitride powder having a thermal diffusivity of from about $0.14 \text{ cm}^2/\text{s}$ to about $0.20 \text{ cm}^2/\text{s}$.

Another aspect of the present invention relates to boron nitride powder having a thermal diffusivity of from about $0.14 \text{ cm}^2/\text{s}$ to about $0.20 \text{ cm}^2/\text{s}$.

20 The method of the present invention produces high thermal diffusivity boron nitride powder which will exhibit high thermal conductivity when used as a filler for thermal management applications, e.g., in composites, polymers, and fluids. The resulting high thermal diffusivity boron nitride powder can also be used in composite polymers and metals for friction applications. Moreover, the resulting high
25 thermal diffusivity boron nitride powder can be used as precursor feed stock material in the conversion of hexagonal boron nitride to cubic boron nitride.

BRIEF DESCRIPTION OF THE DRAWINGS

30 Figure 1 is a graphic showing the structure of hexagonal boron nitride.

DETAILED DESCRIPTION OF THE INVENTION

The present invention relates to a method for making boron nitride powder having a thermal diffusivity of from about $0.14 \text{ cm}^2/\text{s}$ to about $0.20 \text{ cm}^2/\text{s}$.

- 5 This method involves pressing high purity, hexagonal boron nitride having an average platelet size of at least 2 microns into a compacted form, sintering the compacted form of boron nitride to form a sintered body, and crushing the sintered body under conditions effective to produce boron nitride powder having a thermal diffusivity of from about $0.14 \text{ cm}^2/\text{s}$ to about $0.20 \text{ cm}^2/\text{s}$.

- 10 Hexagonal boron nitride is an inert, lubricious ceramic material having a platey hexagonal crystalline structure (similar to that of graphite) ("h-BN"). The well-known anisotropic nature of h-BN can be easily explained by referring to Figure 1, which shows hexagons of an h-BN particle. The diameter of the h-BN particle platelet is the dimension shown as D in Figure 1, and is referred to as the a-direction.
- 15 BN is covalently bonded in the plane of the a-direction. The particle thickness is the dimension shown as L_c , which is perpendicular to diameter and is referred to as the c-direction. Stacked BN hexagons (i.e., in the c-direction) are held together only by Van der Waals forces, which are relatively weak. When a shearing force greater than the weak Van der Waals force is imparted across of the planes of BN hexagons, the
- 20 weak Van der Waals force is overcome and the planes slide relative to each other. The relative ease with which these planes of BN slide against each other may be one of the reasons for the high lubricity of h-BN.

- Preferably, the h-BN is a powder having a highly ordered hexagonal structure. Such powders have a crystallization index (Hubacek, "Hypothetical Model of Turbostratic Layered Boron Nitride," J. Cer. Soc. of Japan, 104:695-98 (1996),
- 25 which is hereby incorporated by reference) of at least 0.12 (quantification of highly hexagonal h-BN) and, preferably, greater than 0.15. Preferably, the h-BN powder has a crystallinity of about 0.20 to about 0.55, most preferably, from about 0.30 to about 0.55. Typically, this starting powder is produced by a "high fire" treatment of a raw,
- 30 essentially turbostratic (amorphous) boron nitride powder (see Hagio et al., "Microstructural Development with Crystallization of Hexagonal Boron Nitride," J. Mat. Sci. Lett. 16:795-798 (1997), which is hereby incorporated by reference) to produce what is conventionally referred to as "high purity hexagonal boron nitride."

In a preferred embodiment, a fine turbostratic BN powder having a crystallization index of less than 0.12 is heat treated in nitrogen at about 1400 to 2300 °C for about 0.5-12 hours. This heat treatment typically acts to produce a more coarse h-BN powder, as the fine, <1 µm crystallites, of turbostratic powder particles become more
5 ordered (crystallized) and larger (>1 micron) during the heat treatment.

Preferably, the particles of the h-BN starting material have an average particle-platelet size of from about 2 µm to about 20 µm, more preferably between about 2 µm and 12 µm, and most preferably, between about 4 µm and about 12 µm. As used herein, "particle size" or "diameter" of the h-BN particle platelet is the
10 dimension shown as D in Figure 1. This is typically measured by scanning electron microscopy and laser scattering techniques using, e.g., a Leeds & Northrup Microtrac X100 (Clearwater, FL).

In another embodiment, the h-BN starting material has an oxygen content of from about 0 wt.% to about 1.0 wt.%, preferably, from about 0 wt.% to
15 about 0.5 wt.%. The use of h-BN starting material with a low oxygen content produces boron nitride powders with a higher tap density. Higher tap density powders have many advantages as fillers in thermal management applications including: higher thermal conductivity, higher powder loading in a matrix; stronger agglomerates of h-BN particles (leading to improved metal adhesion in polymer BN composites); and
20 lower porosity within the agglomerates (which results in less infiltration of polymer resin or liquid into the agglomerate).

In a preferred embodiment, the boron nitride powder having a thermal diffusivity of from about 0.14 cm²/s to about 0.20 cm²/s (i.e., high thermal diffusivity boron nitride powder) has a tap density of from about 0.7 g/cc to about 0.9 g/cc.

25 In yet another embodiment, the h-BN starting material has a surface area of from about 1 m²/g to about 10 m²/g, and more preferably, about 2 m²/g to about 4 m²/g.

The high purity, hexagonal boron nitride starting material may be, but is not limited to, boron nitride powder, boron nitride briquettes, crushed boron nitride
30 briquettes, granulated boron nitride, spray dried boron nitride, or combinations thereof.

In accordance with the present invention, the high purity, hexagonal boron nitride is pressed into a compacted form. Suitable methods for pressing the

hexagonal boron nitride include hot uniaxial pressing, cold uniaxial pressing, hot isopressing, and cold isopressing. Pressing is preferably carried out at a pressure of about 1 ksi to about 60 ksi. Most preferably, the high purity, hexagonal boron nitride is cold isopressed into a compacted form at from about 5 ksi to about 60 ksi.

5 In a preferred embodiment, the compacted form of boron nitride has a thermal diffusivity of from about $0.08 \text{ cm}^2/\text{s}$ to about $0.14 \text{ cm}^2/\text{s}$.

 In another preferred embodiment, the compacted form of boron nitride has a density of between 1.60 g/cc and 1.86 g/cc .

 Preferably, the sintering is carried out at a temperature of at least about
10 1400°C for about 0.5 to about 12 hours, more preferably, for about 1 to about 8 hours. Further, the sintering is preferably carried out at from about 1400°C to about 2300°C , more preferably, from about 1700°C to 2300°C , most preferably, from about 1950°C to about 2100°C . Suitable atmospheres for sintering include inert gas, nitrogen, and argon. In one embodiment, the sintering is carried out in a vacuum. In an another
15 embodiment, the sintering is carried out under conditions of at least 1 atmosphere of pressure.

 In one embodiment, the sintered body has a density of about 1.4 g/cc to about 1.7 g/cc . The resulting powder tap density preferably ranges from 0.7 g/cc to 0.9 g/cc .

20 In accordance with the present invention, the sintering step improves the thermal diffusivity and, thus, thermal conductivity of the resulting boron nitride powder. Although not wishing to be bound by theory, it is believed that during sintering, individual grains of boron nitride grow into each other to form an interconnected network. The interconnectivity of the resulting sintered body results in
25 increased thermal diffusivity and increased thermal conductivity. Preferably, after sintering the thermal diffusivity increases above the compacted green body to about $0.18 \text{ cm}^2/\text{sec}$.

 Suitable methods for crushing the sintered body include jaw crushing and roll crushing. The sintered body is crushed into agglomerates of high thermal
30 diffusivity boron nitride having a desired agglomerate size. As used herein, an agglomerate means a collection of boron nitride particles bonded together. Preferably, the sintered body is crushed into agglomerates of high thermal diffusivity boron nitride of from about 20 microns to about 500 microns. Most preferably, the

majority of boron nitride agglomerates have an average agglomerate size at least 30 to 105 microns.

In another embodiment, the high thermal diffusivity boron nitride powder is classified under conditions effective to obtain a desired agglomerate size distribution. Suitable methods for classification include screening, air classifying, and elutriation, (see Chem. Eng. Handbook, Perry & Chilton, 5th Ed., McGraw-Hill (1973), which is hereby incorporated by reference). As such classification methods are well known in the art, they will only be discussed briefly herein.

Screening is the separation of a mixture of various sized solid particles/agglomerates into two or more portions by means of a screening surface. The screening surface has openings through which the smaller particles/agglomerates will flow, while the larger particles/agglomerates remain on top. This process can be repeated for both the coarse and small particle/agglomerate size streams, as many times as necessary, through varying screen openings to obtain a classification of particles/agglomerates into a desired particle/agglomerate size range.

Air classifiers rely upon air drag and particle inertia, which depends upon particle/agglomerate size, to facilitate the separation of fine particles/agglomerates from coarse particles/agglomerates.

One design for elutriation is a vertical gravity type elutriator, where fluid flowing up through a column carries fine particles/agglomerates smaller than a critical size. The critical size is determined by the settling velocity of the particle/agglomerate in the fluid.

A desired agglomerate range or agglomerate size distribution (ASD) is determined by the intended use of the high thermal diffusivity boron nitride powder. For example, for compliant interface pads, where the polymer is a low durometer silicone rubber, the desired ASD is such that the coarsest agglomerate diameter is smaller than the thickness of the interface pad. For situations in which viscosity control is important in either processing or in the application of a fluid product that is thixotropic, fine particles, e.g., up to 38 microns, are reduced in concentration or removed entirely, which leads to improved processing and wetting of the boron nitride by a polymer and provides a mixture that flows more freely.

Preferably, the ASD is 30 to 125 microns (more preferably 74 to 125 microns, most preferably 74 to 105 microns), or 20 to 74 microns (more preferably 38

to 74 microns, most preferably 38 to 53 microns), or 10 to 38 microns (more preferably 20 to 38 microns).

The above-described method of the present invention provides an efficient technique for preparing high thermal diffusivity boron nitride powder as it requires only a single crushing step, a single sintering step, and a single pressing step. This is in contrast to prior art methods (see, e.g., U.S. Patent No. 5,898,009 to Shaffer et al. and U.S. Patent No. 6,048,511 to Shaffer et al., which are hereby incorporated by reference) which require numerous crushing and pressing steps, but no sintering steps.

The method of the present invention produces high thermal diffusivity boron nitride powder which can be used as a filler for thermal management applications, e.g., in composites, polymers, and fluids. Polymer systems may include melt-processable polymers, polyesters, phenolics, silicone polymers (e.g., silicone rubbers), acrylics, waxes, thermoplastic polymers, low molecular weight fluids, and epoxy molding compounds. The thermal conductivity of the resulting polymer-boron nitride composite or fluid is determined by loading, dispersion, and other factors. The resulting high thermal diffusivity boron nitride powder can also be used in composite polymers and metals for friction applications. Moreover, the resulting high thermal diffusivity boron nitride powder having a tap density of from about 0.7 g/cc to about 0.9 g/cc can be used as precursor feed stock material in the conversion of hexagonal boron nitride to cubic boron nitride. In the conversion of high purity hexagonal boron nitride to cubic boron nitride, the compacted form of boron nitride is subjected to extremely high pressures and temperatures within the stable region of the cubic boron nitride phase diagram. The density of the boron nitride pellets is significant to the economics of the cubic boron nitride conversion process.

Another aspect of the present invention relates to a boron nitride powder having a thermal diffusivity of from about $0.14 \text{ cm}^2/\text{s}$ to about $0.20 \text{ cm}^2/\text{s}$.

Preferably, the boron nitride powder has a tap density of from about 0.7 g/cc to about 0.9 g/cc.

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EXAMPLES

Example 1 – Preparation of Boron Nitride (BN) Powder Using Low Surface Area BN Starting Material

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Boron nitride having a surface area of 2 to 4 m²/g, an average agglomerate size less than 210 microns, a primary platelet size of 6 to 12 microns, an oxygen content of less than 1%, and a B₂O₃ content of less than 0.1%, was isopressed at 20 ksi into a compacted form (all experiments described herein were repeated
10 twice). The compacted form of boron nitride had a green density of between 1.66 and 1.70 g/cc. The thermal diffusivity was measured by laser flash technique (using an Appollo Laser, Model M22) and was found to be between 0.085 and 0.14 cm²/sec. The compacted green bodies were then sintered at 2000 °C for 0.5 to 2 hours. The density of the sintered body was found to have decreased to 1.42 to 1.55 g/cc. The
15 thermal diffusivity was measured again by the same technique and found to have increased to 0.182 cm²/sec. The sintered body was then crushed in a roll mill (Model 666 "F" Gran-U-Lizer, Modern Process Equipment, Chicago, IL). The tap densities of powders after sintering were in the range of 0.74 to 0.81 g/cc.

Example 2 – Preparation of Starting BN Powder

A submicron, dried, filter cake made up of boron nitride powder synthesized at temperatures below 1400 °C (see, e.g., Paine et al., "Synthetic Routes to Boron Nitride," Chem. Rev., 90:73-91 (1990), which is hereby incorporated by
25 reference) was heat-treated at approximately 2000 °C for about 12 hours. The resulting sintered boron nitride powder cake had a bulk density of about 0.85 g/cc, a surface area of between 2 and 4 m²/g, and an oxygen content of less than 0.5 wt.%. The cake was subsequently roll crushed to two types of powder: agglomerates ranging from 30 to 700 microns and fines less than 30 microns. These powders served as BN
30 starting material for sintering.

Example 3 – Preparation of BN Powder Using Fines Starting Material

The fines of Example 2 were isopressed at 20 ksi resulting in a compacted form having a green density of 1.74 g/cc. This green compacted form was
35 then sintered at about 2050 °C for about 2 hours, after which the sintered density was

measured to be 1.60 g/cc. The tap density of the powder prepared by roll crushing and classifying to an agglomerate size distribution between 30 and 105 microns was found to be approximately 0.83 g/cc.

5 **Example 4 – Preparation of BN Powder Using Agglomerate Starting Material**

Agglomerated starting BN powder having agglomerates of BN particles having an average agglomerate size of about 400 to 700 microns, as described in Example 2, was isopressed and sintered as described in Example 3. The resulting compact green density was measured to be 1.66 g/cc. The sintered compact
10 density was measured to be 1.56 g/cc. The tap density of powder from this sintered agglomerate was 0.81 g/cc.

Example 5 – Preparation of BN Powder Using a Blend Starting Material

A roll-crushed blend of agglomerates and fines were used as a starting
15 material. The resulting green density of the compacted form after isopressing at 20 ksi was 1.66 g/cc. After sintering at about 2050 °C for 2 hours the sintered density was measured to be 1.52 g/cc. The tap density of 30 to 105 micron agglomerates was found to be about 0.79 g/cc.

Although preferred embodiments have been depicted and described in
20 detail herein, it will be apparent to those skilled in the relevant art that various modifications, additions, substitutions and the like can be made without departing from the spirit of the invention and these are therefore considered to be within the scope of the invention as defined in the claims which follow.